Amendments to the Specification:

Please replace the Abstract with the following amended Abstract at page 59, lines 2-24:

Polymers ~~The invention relates to a polymer~~ comprising units derived from ethylene, said polymer having: a) a Melt Index of from 0.05 to 20 g/10 min as determined by ASTM-1238 Condition E; b) at least 10 per 1000 C-atoms of short chain branches, containing five carbon atoms or less, as determined by C13 NMR, and less than 3.5 mol%, of units derived from a copolymerizable ethylenically unsaturated ester, c) a density of from 0.90 to 0.94 g/cm^3, preferably 0.91 to 0.935 g/cm^3, especially 0.92 to 0.93 g/cm^3 as determined by ASTM D1505, and d) a relaxation time as described herein of at least 10 s. Such polymers ~~are obtainable by polymerization~~ can be obtained by free radical polymerization using a chain transfer agent that incorporates into the polymer chain such as an alpha-olefin, preferably propylene, as a chain transfer agent, preferably in a tubular reactor under circumstances to favor LCB formation in a down stream part of the tubular reactor.

~~The polymer may be used for stretch hood film, preferably as a blown film coextruded tube comprising: a) a core of the above polymer; and b) a skin layer, on each side of the core which may be of the same or different composition, comprising at least 60 wt % of an LLDPE having density of 0.91 to 0.94 g/cm^3 as determined by ASTM-D 1238 Condition E and hexane extractables less than 1.5 wt %, said skin layer containing less than 7500 ppm of anti-block particulates and said film having an elastic recovery after a 100 % stretch of at least 40 % and providing a normalized holding force per 100 μm thickness pre-stretch at 85 % stretch after an initial stretch of 100 % of at least 20 N/50 mm at a deformation rate of less than 10 % of the starting length per second.~~

Please replace the paragraph at page 20, lines 1-8 with the following amended paragraph:

With reference to Figures 1 and 2 in a tubular reactor, a monomer feed of ethylene, vinyl acetate and transfer agent via line 2 is supplied to a primary compressor 4 and hence to a secondary compressor 6. The discharge flow of the secondary compressor 6 is divided in the number of streams required for the front and side streams of the tubular reactor 8 as indicated by arrows Ib to IVb in Figure 2. The flow to the front (upstream end) of the reactor 8 is heated at 10 while the flows to the side stream entry points are cooled at 12. The side stream flows are then fed to injection points along the length of the tubular reactor 8.